

**Amendments to the Claims:**

The following claims will replace all prior versions of the claims in this application (in the unlikely event that no claims follow herein, the previously pending claims will remain):

1-6. (Cancelled)

7. (Currently Amended) A method of producing a vacuum gas oil (VGO), consisting of:

- I) upgrading bitumen ~~a heavy hydrocarbon feedstock~~ by a method comprising:
  - i) providing a particulate heat carrier into an upflow reactor;
  - ii) introducing bitumen ~~the heavy hydrocarbon feedstock~~ into the upflow reactor at at least one location above that of the particulate heat carrier so that a loading ratio of the particulate heat carrier to bitumen ~~the heavy hydrocarbon feedstock~~ is from about 10:1 to about 200:1, wherein the upflow reactor is run at a temperature of from about 300°C to about 700°C;
  - iii) allowing bitumen ~~the heavy hydrocarbon feedstock~~ to interact with the heat carrier with a residence time of less than about 5 seconds, to produce a product stream;
  - iv) separating the product stream from the particulate heat carrier;
  - v) regenerating the particulate heat carrier; and
  - vi) collecting a gaseous and liquid product from the product stream, and
- II) isolating the VGO from the liquid product.

8. (Previously Presented) The method of claim 7, wherein in step ii, the loading ratio is from about 20:1 to about 30:1.

9. (Cancelled)

10. (Previously Presented) The method of claim 7, wherein in step iii, the product stream of a first pyrolysis run is separated into a light fraction and a heavy fraction,

the light fraction is collected from the product stream, and the heavy fraction is recycled back into the upflow reactor for further processing within a second pyrolysis run to produce a second product stream.

11. (Currently Amended) The method of claim 10, wherein the further processing includes mixing the heavier fraction with the particulate heat carrier, wherein the particulate heat carrier of the second pyrolysis run is at a temperature at about, or above, that used in the processing of bitumen ~~the feedstock~~ within the first pyrolysis run.

12. (Currently Amended) The method of claim 11, wherein the heavier fraction is added to unprocessed bitumen ~~feedstock~~ prior to being introduced into the upflow reactor for the second pyrolysis run.

13. (Previously Presented) The method of claim 10, wherein the temperature of the upflow reactor within the first pyrolysis run is from about 300°C to about 590°C, and the temperature of the upflow reactor within the second pyrolysis run is from about 530°C to about 700°C, and wherein the residence time of the second pyrolysis run is the same as, or longer than, the residence time of the first pyrolysis run.

14. (Previously Presented) The method of claim 11, wherein the particulate heat carrier is separated from the second product stream, and a second product is collected from the second product stream.

15. (Previously Presented) The method of claim 10, wherein the product stream of the first pyrolysis run is treated within a hot condenser prior to recovery of the light fraction and the heavy fraction.

16-17. (Cancelled)

18. (Previously Presented) The method of claim 7, wherein the VGO is characterized as comprising a measured aniline point from about 110°F to about 170°F, wherein the measured aniline point is lower than a calculated aniline point.

19. (Currently Amended) A method of producing a vacuum gas oil (VGO), comprising comprising:

- I) upgrading bitumen ~~a heavy hydrocarbon feedstock having a viscosity greater than about 375 at 40°C. (cSt)~~, by a method comprising:
  - i) providing a particulate heat carrier into an upflow reactor;
  - ii) introducing bitumen ~~the heavy hydrocarbon feedstock~~ into the upflow reactor at at least one location above that of the particulate heat carrier so that a loading ratio of the particulate heat carrier to bitumen ~~the heavy hydrocarbon feedstock~~ is from about 10:1 to about 200:1, wherein the upflow reactor is run at a temperature of from about 300°C to about 700°C;
  - iii) allowing bitumen ~~the heavy hydrocarbon feedstock~~ to interact with the heat carrier with a residence time of less than about 5 seconds, to produce a product stream;
  - iv) separating the product stream from the particulate heat carrier;
  - v) regenerating the particulate heat carrier; and
  - vi) collecting a gaseous and liquid product from the product stream; and
- II) isolating the VGO from the liquid product.

20. (Previously Presented) The method of claim 19, wherein in step ii, the loading ratio is from about 20:1 to about 30:1.

21. (Cancelled)

22. (Previously Presented) The method of claim 19, wherein in step iii, the product stream of a first pyrolysis run is separated into a light fraction and a heavy fraction, the light fraction is collected from the product stream, and the heavy fraction is recycled back into the upflow reactor for further processing within a second pyrolysis run to produce a second product stream.

23. (Currently Amended) The method of claim 22, wherein the further processing includes mixing the heavier fraction with the particulate heat carrier, wherein the particulate heat carrier of the second pyrolysis run is at a temperature at about, or

above, that used in the processing of bitumen ~~the feedstock~~ within the first pyrolysis run.

24. (Currently Amended) The method of claim 23, wherein the heavier fraction is added to unprocessed bitumen ~~feedstock~~ prior to being introduced into the upflow reactor for the second pyrolysis run.

25. (Previously Presented) The method of claim 22, wherein the temperature of the upflow reactor within the first pyrolysis run is from about 300°C to about 590°C, and the temperature of the upflow reactor within the second pyrolysis run is from about 530°C to about 700°C, and wherein the residence time of the second pyrolysis run is the same as, or longer than, the residence time of the first pyrolysis run.

26. (Previously Presented) The method of claim 23, wherein the particulate heat carrier is separated from the second product stream, and a second product is collected from the second product stream.

27. (Previously Presented) The method of claim 22, wherein the product stream of the first pyrolysis run is treated within a hot condenser prior to recovery of the light fraction and the heavy fraction.

28. (Previously Presented) The method of claim 19, wherein the VGO is characterized as comprising a measured aniline point from about 110°F to about 170°F, wherein the measured aniline point is lower than a calculated aniline point.

29. (Currently Amended) A method of producing a vacuum gas oil (VGO), consisting of:

- I) upgrading bitumen ~~a heavy hydrocarbon feedstock~~ by a method comprising:
  - i) providing a particulate heat carrier into an upflow reactor, wherein the loading ratio of the particulate heat carrier to bitumen ~~the heavy hydrocarbon feedstock~~ is from about 10:1 to about 200:1, and wherein the upflow reactor is run at a temperature of from about 300°C to about 700°C;

- ii) allowing bitumen ~~the heavy hydrocarbon feedstock~~ to interact with the heat carrier with a residence time of less than about 5 seconds, to produce a product stream;
- iii) collecting a gaseous and liquid product from the product stream;

- II) transporting the liquid product; and
- III) isolating the VGO from the liquid product.

30. (Previously Presented) The method of claim 29, wherein in step ii, the loading ratio is from about 20:1 to about 30:1.

31. (Cancelled)

32. (Previously Presented) The method of claim 29, wherein in step iii, the product stream of a first pyrolysis run is separated into a light fraction and a heavy fraction, the light fraction is collected from the product stream, and the heavy fraction is recycled back into the upflow reactor for further processing within a second pyrolysis run to produce a second product stream.

33. (Currently Amended) The method of claim 32, wherein the further processing includes mixing the heavier fraction with the particulate heat carrier, wherein the particulate heat carrier of the second pyrolysis run is at a temperature at about, or above, that used in the processing of bitumen ~~the feedstock~~ within the first pyrolysis run.

34. (Currently Amended) The method of claim 33, wherein the heavier fraction is added to unprocessed bitumen ~~feedstock~~ prior to being introduced into the upflow reactor for the second pyrolysis run.

35. (Previously Presented) The method of claim 32, wherein the temperature of the upflow reactor within the first pyrolysis run is from about 300°C to about 590°C, and the temperature of the upflow reactor within the second pyrolysis run is from

about 530°C to about 700°C, and wherein the residence time of the second pyrolysis run is the same as, or longer than, the residence time of the first pyrolysis run.

36. (Previously Presented) The method of claim 33, wherein the particulate heat carrier is separated from the second product stream, and a second product is collected from the second product stream.

37. (Previously Presented) The method of claim 32, wherein the product stream of the first pyrolysis run is treated within a hot condenser prior to recovery of the light fraction and the heavy fraction.

38. (Previously Presented) The method of claim 29, wherein the VGO is characterized as comprising a measured aniline point from about 110°F to about 170°F, wherein the measured aniline point is lower than a calculated aniline point.

39. (Currently Amended) The method of claim 29, wherein the upgrading step further comprises introducing bitumen ~~the heavy hydrocarbon feedstock~~ into the upflow reactor at at least one location above that of the particulate heat carrier so that a loading ratio of the particulate heat carrier to bitumen ~~the heavy hydrocarbon feedstock~~ is from about 10:1 to about 200:1, wherein the upflow reactor is run at a temperature of from about 300°C to about 700°C;

40. (Previously Presented) The method of claim 29, wherein the upgrading step further comprises separating the product stream from the particulate heat carrier.

41. (Previously Presented) The method of claim 40, wherein the upgrading step further comprises regenerating the particulate heat carrier.

42. (Previously Presented) The method of claim 29, wherein the transporting step comprises transporting the liquid product to a remote site.

43. (Previously Presented) The method of claim 42, wherein said remote site is a refinery.

44-53. (Cancelled)